

PARTICULATE EMISSION TEST SURVEY

FOR

DUNLOP OIL & MARINE LTD

Project No : 74981-87 (1)

19 November 2013

Global Surface Coatings Covered



ENVIRONMENTAL SERVICES TEST REPORT

- **Project No.** 74981-87 (1)
- **Test Dates** 7 November 2013
- **Report Date** 19 November 2013
 - Client Dunlop Oil & Marine Ltd Moody Lane Pyewipe Grimsby North East Lincolnshire DN31 2SY

FAO Chris Allen

Work requested

Particulate Emission Test Survey

Work carried out by

T. Sullivan Environmental Services

T.J. Glavcier

Approved by

T.J. Glazier, A. Miller Approved Signatory

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PARTICULATE EMISSION TEST SURVEY

1.0 Introduction

This report presents the test procedures, results, conclusions and recommendations of the test survey carried out on 7 November 2013 by Tim Sullivan MCERTS Accreditation No. MM03456.

Dunlop Oil & Marine Ltd have asked PRA to carry out particulate emission testing of the two dust release points. The Bag Filtration Unit which serves LEV 07 (Banbury Mixer & experimental lab), LEV 40 (bulk carbon black hoppers) and LEV's 1, 2, 38 & 39 (powder weighing and Banbury Mixer downchute) and the Banbury Mixer release point.

This test survey will enable Dunlop Oil & Marine Ltd to check their compliance against the particulate emission limits given in process guidance note PG6/28 (11) "Guidance for Rubber".

2.0 Test Procedures

2.1 Location of Sampling Ports

A description of the sampling port location at each release point is given in table 1.0. Diagrams of the stacks and sampling ports are shown in appendix 1.

Table 1Sample point locations

	Release Point	Test Parameters
1.	Bag Filtration Unit	Particulate emission
2.	Banbury Mixer	Particulate emission

2.2 Flow

The gas velocity at release point 2 (Banbury Mixer) was measured using an ellipsoidal nose pitot tube and calibrated micromanometer in accordance with ISO 10780 "Measurement of velocity and volume flowrate of gas streams in ducts".

The gas velocity at the exit grill of release point 1 was too turbulent to measure using a pitot tube and micromanometer, therefore a rotating vane anemometer was used to give an indication of the gas velocity.

The gas temperature was measured using a calibrated digital temperature indicator and K type probe. The temperature was measured at the same sampling points as the flow measurements.

2.3 Particulate Emission

The particulate emission was measured using a gravimetric filter technique in accordance with BS ISO 9096 : 2003 "Manual determination of mass concentration of particulate matter."

For release point 1 (bag filtration unit) the flow did not meet the criteria stated in BS ISO 9096. However indicative flow measurement was taken using a hand held rotating vane anemometer.

For release point 2 (Banbury Mixer) the angle of gas flow was less than 15° with respect to the duct axis, no negative gas flow was found, the minimum pitot static reading was greater than 5 Pa and the ratio of the highest and lowest pitot static readings was less than 3 :1. The temperature across the ducts did not vary by more than 5 % from the mean temperature. Therefore the flow in the sampling plane met the criteria stated in BS ISO 9096.

For release point 1 (bag filtration unit) the duct area was between 0.38 and 1.50 m^2 therefore nine point cumulative sampling at 0.25D, 0.50D and 0.75D along three sample lines was used.

For release point 2 the duct diameter was between 0.35 and 0.70 m therefore five point cumulative sampling at 0.113D, 0.50D and 0.887D along two stack diameters would normally be used. However because the working platform only gave access one side of the duct, it was decided to carry out five point sampling at 0.059D, 0.211D, 0.50D, 0.789D and 0.941D along a single stack diameter. It is considered that this sampling procedure would provide representative sample of the particulate emission.

The particulate sampling train (J.S. Holdings Stack Sampler) was checked for leaks under pressure (i.e. the sampling train was assembled, the sample pump was switched on, the nozzle of the probe was covered and the flow rate was checked to ensure a stable vacuum was maintained). The test showed the sample train was leak free.

The sampled gas was extracted at a rate that ensured the gas velocity at the sampler nozzle was equal to the gas velocity in the stack at the point of sampling (i.e. isokinetic sampling).

One particulate concentration determination was taken for each of the release points in order to sample for longer and try to ensure a measurable weight gain on the filter.

The uncertainty in the particulate concentration due to deviations from BS ISO 9096 was estimated using guidelines given by the Source Testing Association.

3.0 Results

This section presents a summary of the test results. All test results are reported at reference conditions 273 K and 1013 m.bar without correction for water vapour.

The measurements for were taken under what was considered typical production conditions.

The methods for calculating the gas velocity, volume flow, particulate concentration, and isocyanate concentration are shown in appendix 2. The test data for flow, volume sampled, % isokinetic and uncertainty of measurement are shown in appendix 3.

3.1 Flow

The gas velocity and volume flow for each release point are shown in table 2.

Release Point	Date	Gas Velocity (m/s)	Volume Flow at STP (m ³ /h)
1 Bag Filtration Unit	7 November - 10.40	8.10	10669
2 Banbury Mixer	7 November – 13.30	9.48	8853

Table 2 Flow

3.2 Particulate Emission

3.2.1 Release Point 1 – Bag Filtration Unit

The particulate concentration measured at release point 1 is shown in table 3.

Table 3Particulate emission concentration

Test No.	Date/Time	% Isokinetic	Sampling Period (mins)	Weight of Particulate (mg)	Volume Sampled (m ³)	Particulate Conc. (mg.m ⁻³)
1	7 November 10.55	99	81	0.5	1.0238	0.5 ± 0.4

3.2.2 Release Point 2 – Banbury Mixer

The particulate concentration measured at the Banbury Mixer extract duct is shown in table 4.

Table 4Particulate emission concentration

Test No.	Date/Time	% Isokinetic	Sampling Period (mins)	Weight of Particulate (mg)	Volume Sampled (m ³)	Particulate Conc. (mg.m ⁻³)
1	7 November 13.45	95	50	0.5	0.7139	0.7 ± 0.5

3.2.3 Particulate Blank

The blank particulate concentration is shown in table 5.

Table 5Blank Particulate emission concentration

Test No.	Date	Weight of Blank (mg)	Average Volume Sampled (m ³)	Blank Particulate Conc. (mg.m ⁻³)	
1	7 November	0.3	0.8688	0.3	

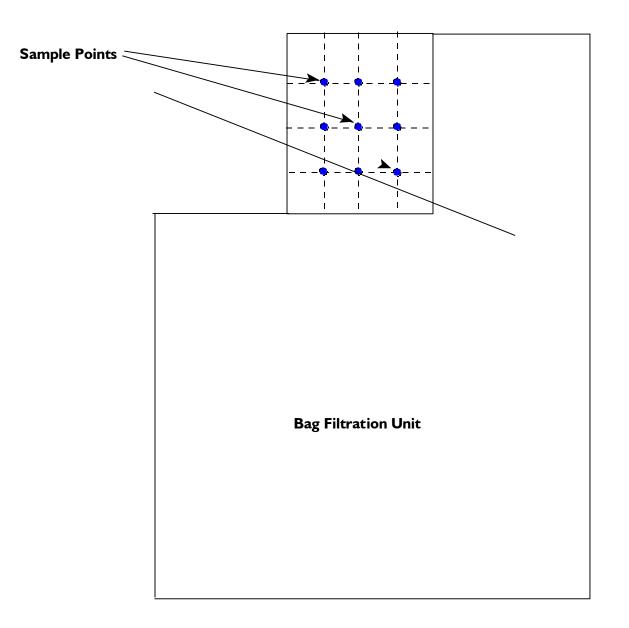
4.0 Conclusions

The particulate emission concentration (0.5 mg.m⁻³) from release point 1 - Bag Filtration Unit - is below the emission limit of 10 mg.m⁻³ for the storage, handling or mixing of carbon black as set out in process guidance note PG6/28 (04) "Guidance for Rubber".

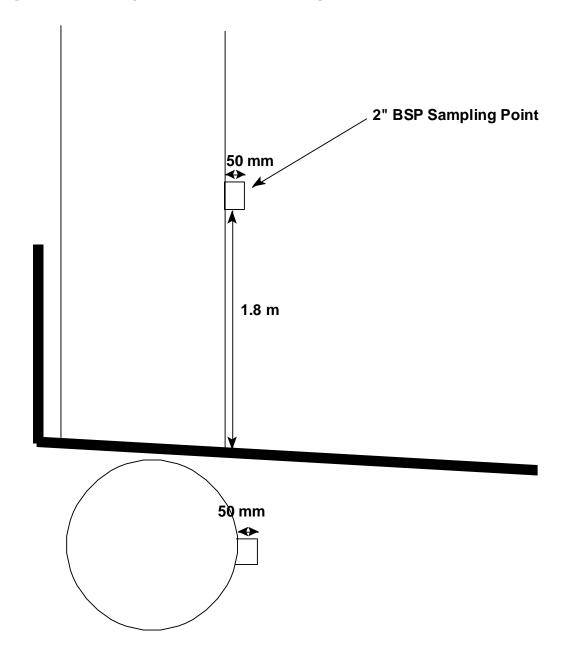
The particulate emission concentration (0.7 mg.m⁻³) from release point 2 - Banbury Mixer is below the emission limit of 50 mg.m⁻³ for any source other than carbon black.

APPENDIX 1

Diagram 1.0 Sampling Points for Bag Filtration Unit







APPENDIX 2

Calculations

1.0 Gas Flow Calculations

$$V_{\text{STP}} = K_p \times 1.29 \times \sqrt{H_V}$$

where
$$V_{STP}$$
 = gas velocity at STP (m/s)
 K_p = pitot correction factor
= 0.996
1.29 = gas density at 273 K and 1013 m.bar
 H_V = mean velocity pressure (Pa)

ii) Actual gas velocity (V_A)

$$V_{A} = V_{STP} \times \sqrt{\frac{T}{273}} \times \frac{1013}{0.01(H_{s}) + B}$$

where V_{STP} = gas velocity at STP (m/s) T = temperature of gas in duct (K) H_s = static pressure (Pa) B = atmospheric pressure (m.bar)

iii) Actual Gas Flowrate (Q)

 $\begin{array}{rcl} Q &= V_A \ x \ A \ x \ 3600 \\ \\ \mbox{where } Q &= \mbox{gas flowrate } (m^3/h) \\ \\ V_A &= \mbox{actual gas velocity } (m/s) \\ \\ A &= \ X \ \mbox{sectional area of vent } (m^2) \end{array}$

iv) Gas flowrate at STP (Q_{STP})

 $Q_{STP} = Q \times \frac{273}{T} \times \frac{B}{1013}$ where Q = gas flowrate at STP (m³/h) T = temperature of gas in stack (K) B = barometric atmospheric pressure (m.bar)

2.0 Particulate Emission Concentration

2.1 Weight of Particulate

a) weight of particulate on filter = $(F_2 - F_1) - (C_2 - C_1)$ where F_2 = final weight of test filter (g) F_1 = initial weight of test filter (g) C₂ = final weight of control filter (g) = initial weight of control filter (g) C_1 b) weight of particulate in washings = $(E_2 - E_1) - (C_2 - C_1)$ where E_2 = final weight of evaporated washing + dish (g) E₁ = initial weight of dish (g)C₂ = final weight of control dish (g) = initial weight of control dish (g) C_1 c) total weight of particulate = a + b 2.2 **Volume Sampled** a) registered volume sampled (V_R) = $M_2 - M_1$ where M_2 = final gas meter reading (m³) M_1 = initial gas meter reading (m³) b) true volume sampled (V_T) $= V_R x (100 x R_E)$ where V_R = registered volume (m³) R_E = gas meter correction factor = 0.988c) true volume sampled to STP $= V_T \times 273 \times B$ T 1013 where V_{T} = true volume sampled (m³) 273 = standard temperature (K)

T = gas temperature in stack (K)

1013 = standard atmospheric pressure (m.bar)

B = atmospheric pressure (m.bar)

2.3 Particulate Concentration

 $mg.m^{-3}_{(particulate)} = \frac{W_t}{V}$

where W_t = total weight of particulate captured V = true volume of gas sampled corrected to STP

2.4 Isokinetic Sampling

% Isokinetic = <u>gas velocity at nozzle (m/s)</u> x 100 gas velocity at sample point in duct (m/s)

a) gas velocity at nozzle= V_T (m/s) $A_N \times T_S$

where V_{T}	= true volume of gas sampled at actual
	temperature & pressure. (m ³)
A _N	= nozzle area (m ²)
Τs	= sampling time (secs)

b) gas velocity at sample point in duct
=
$$1.29 \times \sqrt{H_v} \times \sqrt{\frac{T}{273} \times \frac{1013}{B}}$$

where 1.29 = gas density at 273 K and 1013 m.bar $\sqrt{H_V}$ = mean square root of the velocity pressure (Pa) T = temperature of gas in duct (K) B = atmospheric pressure (m.bar)

3.0 Blank Concentration

3.1 Weight of Particulate

a) weight of particulate on blank filter = $(B_2 - B_1) - (C_2 - C_1)$

where B_2 = final weight of blank filter (g)

B₁ = initial weight of blank filter (g)

C₁ = initial weight of control filter (g)

b) weight of particulate in blank washings = $(W_2 - W_1) - (C_2 - C_1)$

where W_2 = final weight of evaporated blank washing + dish (g)

- W₁ = initial weight of dish (g)
- C₂ = final weight of control dish (g)
- C₁ = initial weight of control dish (g)

c) total weight of blank particulate $(M_B) = a + b$

3.2 Volume Sampled

a) average volume sampled $(V_A) = \underbrace{V_1 + V_n}_n$ where $V_1 =$ volume of gas sampled corrected to STP for test 1(m³) $V_n =$ volume of gas sampled corrected to STP for test n (m³)

3.3 Blank Particulate Concentration

Blank Concentration (mg.m⁻³) = $\underline{M}_{\underline{B}}$ V_A

> where M_B = mass of blank (µg) V_A = average volume sampled at STP from daily tests (m³)

APPENDIX 3

Test Data

1.0 FLOW MEASUREMENTS

Dunlop Oil & Marine Ltd

Project No : 74981-87 (1)

Release Point 1 - Bag Filtration Unit

Date: Time: Gas temperature (K) Atmospheric pressure (m.bar) Duct Dimensions (m) Area (m2)		07/11/2013 10.40 297 1008 0.8 x 0.5 0.4000	
	Face Velocity		Average Face Velocity
	(m/s)		(m/s)
8.9	5.7	6.5	8.10
8.6	8.5	9.7	
9.8	8.3	6.9	
Gas flowrate (m3	/h)	11664	
Gas flowrate at S	TP (m3/h)	10669	

1.0 FLOW MEASUREMENTS

Dunlop Oil & Marine Ltd

Project No: 74981-87 (1)

Release Point 2 - Banbury Mixer

Date: Time: Gas temperature Atmospheric pres Static pressure (r Duct Dimensions	ssure (m.bar) n.bar)	07/09/2013 13.30 296 1008 0.42 0.6		
Area (m2)		0.2827		
Distance Along Sample Line 0.059D 0.211D 0.500D 0.789D 0.941D	Vel. Pressure Hv (Pa) 30 34 45 75 75 75	Sqrt Hv 5.48 5.83 6.71 8.66 8.66	Average Sqrt Hv (Pa) 7.07	Gas Velocity. (m/s) 9.48
Gas flowrate (m3 Gas flowrate at S		9646 8853		

2. PARTICULATE EMISSION: VOLUME SAMPLED

Standard Temperature (K) =	273
Standard Pressure (m.bar) =	1013

2.1 Release Point 1 - Bag Filtration Unit

Test	Date	Time	Temp	Pressure	Initial Gas Meter	Final Gas Meter	Sampled Volume	True Volume	Volume at STP
			К	m.bar	m3	m3	m3	m3	m3
1	07-Nov	10.55	301	1008	725.2581	726.4063	1.1482	1.1344	1.0238

2.2 Release Point 2 - Banbury MIxer

Test	Date	Time	Temp	Pressure	Initial Gas Meter	Final Gas Meter	Sampled Volume	True Volume	Volume at STP
			К	m.bar	m3	m3	m3	m3	m3
1	07-Nov	13.45	303	1008	726.4130	727.2189	0.8059	0.7962	0.7139

3. PARTICULATE EMISSION: WEIGHT COLLECTED

Dunlop Oil & Marine Ltd

Project No: 74981-87 (1)

3.1 Release Point 1 - Bag Filtration Unit

Test	Date	Time	0				Total Collected
			Filter (mg)	Control (mg)	on Filter (mg)	in Washing (mg)	(mg)
1	07-Nov	10.55	0.1	0.0	0.1	0.4	0.5

3.2 Release Point 2 : Banbury Mixer

Test	Date	Time	Weight on	Weight on	Particulate	Particulate	Total Collected
			Filter	Blank Filter	on Filter	in Washing	
			(mg)	(mg)	(mg)	(mg)	(mg)
1	07-Nov	13.45	0.2	0.0	0.2	0.3	0.5

3.3 Blank 1

Test	Date	Time	Weight on Filter	Weight on Blank Filter	Particulate on Filter	Particulate in Washing	Total Collected
1	07-Nov	14.50	(mg) 0.2	(mg) 0.0	(mg) 0.2	(mg) 0.1	(mg) 0.3

4. PARTICULATE EMISSION: CALCULATION OF % ISOKINETIC SAMPLING

Dunlop Oil & Marine Ltd

Project No : 74981-87 (1)

Standard Temperature (K)273Standard Pressure (m.bar)1013

4.1 Release Point 1 - Bag Filtration Unit

 Test 1
 07-Nov-13
 10.55

 Temp =
 301

 Press =
 1008

	Velocity	Nozzle	Nozzle	Sampling	Time	Initial gas	Final gas	Sampled	True	Velocity	SQRT	Velocity	%
	pressure	Size	Area	Flowrate	Sampled	meter	meter	Volume	Volume	at nozzle	Ηv	in Duct	isokinetic
	(Pa)		(m2)	(litres/min)	(secs)	(m3)	(m3)	(m3)	(m3)	(m/s)	(Pa)	(m/s)	
Test 1	37.5	0.006	2.827E-05	13.78	4860	725.2581	726.4063	1.1482	1.1344	8.26	6.12	8.31	99

4.2 Release Point 2 - Banbury Mixer

Test 1 07-Nov-13 13.45 Temp = 303 Press = 1008

Sample	Velocity	Nozzle	Nozzle	Sampling	Time	Initial gas	Final gas	Sampled	True	Velocity	SQRT	Velocity	%
Point	pressure	Size	Area	Flowrate	Sampled	meter	meter	Volume	Volume	at nozzle	Ηv	in Duct	isokinetic
	(Pa)		(m2)	(litres/min)	(secs)	(m3)	(m3)	(m3)	(m3)	(m/s)	(Pa)	(m/s)	
Test 1	52.8	0.006	2.827E-05	15.5	3000	726.4130	727.2189	0.8059	0.7962	9.39	7.27	9.87	95

5.0 Uncertainty calculation for EN 13284 Determination of low range mass concentration of dust, Manual Gravimetric Method

v15									
5.1 Bag Filter- Test 1						Measurement Equa	ation		
Limit value (ELV)		mg.m ^{°°}	Reference oxygen		% by volume	$c = \frac{m}{f} f$			
Measured concentration	0.50	mg.m ⁻³ (at reference conditions)			-	$c = \frac{m}{V} f_c$			
Measured Quantities	Symbol	Value	Standard uncertainty		Units	Uncertainty as per	centage	Uncertainty at lv	Requirement of st
Sampled Volume	V _m	1.1344	uVm	0.001	m³		0.0	9	<=2%
Sampled gas Temperature			uTm		k	1	0.6	6	<=1%
Sampled gas Pressure	ρ _m		uρ _m	1	kPa	1	0.9	9	<=1%
Sampled gas Humidity	H _m		uHm	1	% by volume	1	1.0	0	<=1%
Oxygen content	0 _{2,m}		uO _{2,m}	0.1	% by volume	#DIV/0!			<=5%
Mass particulate	m			0.18	mg	1	36.4	3 1.82	<5% of limit value
Note - Sampled gas humidi	ity, temperatu	re and pressure are values at the gas	meter			1			
Leak	L	. 2			%		2.0	0	<=2%
Uncollected Mass	UCM	0			mg			0	<=10%
(Instack filter - no rinse)									
Intermediate calculations									
Factor for std conds	fs								
uncertainty components	symbol	•		u (in units of fs)					
	ρ _m	0.009		0.009					
	H _m	0.009		0.009		$f_s = \frac{(100 - H_m)}{100} \frac{273}{T_m} \frac{\rho_m}{101.3}$			
	Tm	0.003		0.006		$100 I_m 101.3$			
	ufs			0.014			1.5	6	
Corrected volume	V	1.02	uV	0.016	m³	$V = V_m f_s$	1.5	6	
Factor for O2 correction	fc	1.00							
uncertainty components	symbol			u		$21 - O_{2,ref}$			
	0 _{2,m}	-		0.005		$f_{c} = \frac{21 - O_{2,ref}}{21 - O_{2,m}}$			
Factor for O2 Correction	ufc			0.005		2,00	0.4	8	
									_
Parameter		Value		Sensitivity coeff	Uncertainty contril		tainty as 9		
Corrected Volume (standard cor	nc V	1.02	m	0.40	0.01	mg m ⁻³	15	6 %	

Parameter		value Units	Sensitivity coeff	Uncertainty contribution	Uncertainty as %
Corrected Volume (standard conc	V	1.02 m ³	0.49	0.01 mg.m ⁻³	1.56 %
Mass	m	0.50 mg	1.00	0.18 mg.m ⁻³	36.43 %
Factor for O2 Correction	fc	1.00	0.50	0.00 mg.m ⁻³	0.48 %
Leak	L	0.01 mg.m ⁻³	1.00	0.01 mg.m ⁻³	1.15 %
Uncollected mass	UCM	0.00 mg	1.00	0.00 mg.m ⁻³	0.00 %
Combined measurement uncertaint	ty			0.18 mg.m ⁻³	
Expanded uncertainty as percentag	e of measured value	72.96	% measured of value	expressed with a level of confidence of 95% (Using a coverage factor k=2)	
Expanded uncertainty in units of me	easurement	0.36	mg.m⁻⁵		
Expanded uncertainty as percentag	e of limit value	3.65	% ELV		

Note:

Enter values into green boxes

Developed for the STA by R Robinson, NPL

5.0 Uncertainty calculation for EN 13284 Determination of low range mass concentration of dust, Manual Gravimetric Method

v15								
5.2 Banbury Mixer- Tes	st 1					Measurement Equation	on	
Limit value (ELV)		mg.m ^{°3}	Reference oxygen		% by volume	$c = \frac{m}{m} f$		
Measured concentration	0.70	mg.m ⁻³ (at reference conditions)			-	$c = \frac{m}{V} f_c$		
Measured Quantities	Symbol	Value	Standard uncertainty		Units	Uncertainty as percer	ntage Uncertainty at	lv Requirement of st
Sampled Volume	, V _m	0.7962	uV _m	0.001	m³		0.13	<=2%
Sampled gas Temperature	T _m	303	uTm		k		0.66	<=1%
Sampled gas Pressure	ρ _m	100.8	uρ _m	1	kPa		0.99	<=1%
Sampled gas Humidity	H _m	0	uH _m	1	% by volume		1.00	<=1%
Oxygen content	0 _{2,m}		uO _{2,m}	0.1	% by volume	#DIV/0!		<=5%
Mass particulate	m	0.5	um	0.18	mg		36.42 2.55	<5% of limit value
Note - Sampled gas humidit	ty, temperatu	e and pressure are values at the gas	meter		•			
Leak	L	2			%		2.00	<=2%
Uncollected Mass	UCM	0			mg		0	<=10%
(Instack filter - no rinse)								
Intermediate calculations								
Factor for std conds	fs							
uncertainty components	symbol	sensitivity coeff		u (in units of fs)				
	ρ _m	0.009		0.009				
	H _m	0.009		0.009		$f_s = \frac{(100 - H_m)}{100} \frac{273}{T_m} \frac{\rho_m}{101.3}$		
	T _m	0.003		0.006		$100 I_m 101.3$		
	ufs			0.014			1.56	
Corrected volume	V	0.71	uV	0.011	m³	$V = V_m f_s$	1.56	
Factor for O2 correction	fc	1.00						
uncertainty components	symbol	sensitivity coeff		u		$21 - O_{2 ref}$		
,	0 _{2,m}	0.05		0.005		$f_c = \frac{21 - O_{2,ref}}{21 - O_{2,m}}$		
Factor for O2 Correction	ufc	1.00		0.005		2,11	0.48	
Parameter		Value	Units	Sensitivity coeff	Uncertainty cont	ribution Uncertain	ntv as %	
Corrected Volume (standard con	c V			0.98)1 mg.m ⁻³	1.56 %	
Mass	m			1.40		25 mg.m ⁻³	36.42 %	

ombined measurement uncertainty 0.26 mg.m ³											
expressed with a level of confidence of 95% (Using a coverage factor k=2)											

Note: Enter values into green boxes



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PRA Coatings Technology Centre, 14 Castle Mews, High Street, Hampton, Middlesex TW12 2NP, UK T: +44 (0)20 8487 0800 F: +44 (0)20 8487 0801 E: coatings@pra-world.com