STACK EMISSIONS MONITORING REPORT



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Grimsby Coated Stone
Gilbey Road
Pyewipe
Grimsby
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DN31 2SJ

Permit Reference: DEFRA Process Guidance Note: PG 3/15 (12)

> Release Point: Coating Plant

Sampling Date(s): 19th October 2018

SOCOTEC UK Job Number:	LNO 14547
Report Date:	5th November 2018
Version:	1
Report By:	Andy Hegarty
MCERTS Number:	MM 03 397
MCERTS Level:	MCERTS Level 2 - Team Leader
Technical Endorsements:	1, 2, 3 & 4
Report Approved By:	Dave Armitage
MCERTS Number:	MM 04 516
Business Title:	MCERTS Level 2 - Team Leader
Technical Endorsements:	1, 2, 3 & 4
Signature:	DAmy





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MONITORING OBJECTIVES

CEMEX UK Materials Limited operates a roadstone coating process at Gromsby which is subject to DEFRA Process Guidance Note PG 3/15 (12), under the Environmental Permitting Regulations 2010.

SOCOTEC UK LTD were commissioned by CEMEX UK Materials Limited to carry out stack emissions monitoring to determine the release of prescribed pollutants from the following Plant under normal operating conditions.

The results of these tests shall be used to demonstrate compliance with a set of emission limit values for prescribed pollutants as specified in the Plant's DEFRA Process Guidance Note, PG 3/15 (12).

<u>Plant</u>

Coating Plant

Operator

CEMEX UK Materials Limited Grimsby Coated Stone Gilbey Road Pyewipe Grimsby Lincolnshire DN31 2SJ

DEFRA Process Guidance Note: PG 3/15 (12)

Stack Emissions Monitoring Test House

SOCOTEC UK - Stockport Laboratory Unit 5 Crown Industrial Estate Kenwood Road Stockport SK5 6PH UKAS and MCERTS Accreditation Number: 1015

Opinions and interpretations expressed herein are outside the scope of UKAS accreditation. MCERTS accredited results will only be claimed where both the sampling and analytical stages are UKAS accredited. This test report shall not be reproduced, except in full, without written approval of SOCOTEC UK LTD.



EMISSIONS SUMMARY					
Parameter	Units	Result	Calculated Uncertainty +/-	Limit	MCERTS accredited result
Total Particulate Matter Particulate Emission Rate	mg/m³ g/hr	30 463	1.2 18.5	50 -	1
Moisture	%	2.6	0.09	-	1
Stack Gas Temperature	°C	78	-	-	
Stack Gas Velocity	m/s	19.3	0.49	-	
Gas Volumetric Flow Rate (Actual)	m³/hr	19667	1019	-	
Gas Volumetric Flow Rate (STP, Wet)	m³/hr	15524	804	-	-
Gas Volumetric Flow Rate (STP, Dry)	m³/hr	15120	783	-	
Gas Volumetric Flow Rate at Reference Conditions	m³/hr	15524	804	-	

ND = None Detected,

Results at or below the limit of detection are highlighted by bold italic text.

The above volumetric flow rate is calculated using data from the preliminary survey. Mass emissions for non isokinetic tests are calculated using these values. For all isokinetic testing the mass emission is calculated using test specific flow data and not the above values.

Reference conditions are 273K, 101.3kPa without correction for water vapour



MONITORING TIMES								
Parameter Sampling Date(s) Sampling Times Sampling Duration								
Total Particulate Matter Run 1	19 October 2018	08:29 - 09:01	32 minutes					
Total Particulate Matter Run 2	19 October 2018	09:15 - 09:47	32 minutes					
Preliminary Stack Traverse	19 October 2018	08:12	-					



PROCESS DETAILS

Parameter	Process Details
Description of process	Roadstone Coating
Continuous or batch	Continuous
Product Details	6mm, 10mm & 20mm
Part of batch to be monitored (if applicable)	When mixing
Normal load, throughput or continuous rating	30 - 40t/hr
Fuel used during monitoring	Kerosine
Abatement	Bag Filter
Plume Appearance	Plume Visible



Monitoring Methods

The selection of standard reference / alternative methods employed by SOCOTEC UK is determined, wherever possible by the hierarchy of method selection outlined in Environment Agency Technical Guidance Note (Monitoring) M2.

MONITORING METHODS							
Species	Method	SOCOTEC UK	UKAS Lab	MCERTS	Limit of	Calculated	
	Standard Reference Method /	Technical	Number	Accredited	Detection	MU	
	Alternative Method	Procedure		Method	(LOD)	+/- %	
TPM	SRM - BS EN 13284-1	AE 104	1015	Yes	0.46 mg/m ³	4%	
H ₂ O	SRM - BS EN 14790	AE 105	1015	Yes	0.02%	3.4%	
Velocity	SRM - BS EN ISO 16911-1	AE 154	1015	Yes	5 Pa	2.5%	
Volumetric Flow Rate	SRM - BS EN ISO 16911-1	AE 154	1015	Yes	-	5.2%	

BS EN 14790 has been validated over a range of 4 - 40%. It is however the prefered method of the Environment Agency for concentrations below 4%



Analytical Methods

The following tables list the analytical methods employed together with the custody and archiving details:

	SAMPLING METHODS WITH SUBSEQUENT ANALYSIS							
Species	Analytical Technique	Analytical Procedure	UKAS Lab Number	UKAS Accredited Lab Analysis	Analysis Lab	Sample Archive Location	Archive Period	
TPM	Gravimetric	AE 106	1015	Yes	SOCOTEC UK (Stockport)	SOCOTEC UK (Stockport)	8 Weeks	

	ON-SITE TESTING						
Species	Analytical Technique	Analytical Procedure	UKAS Lab Number	MCERTS Accredited Analysis	Laboratory	Data Archive Location	Archive Period
H ₂ 0	Gravimetric	AE 105	1015	Yes	SOCOTEC UK (Stockport)	-	-



SAMPLING LOCATION						
Sampling Plane Validation Criteria	Value	Units	Requirement	Compliant	Method	
Lowest Differential Pressure	275	Pa	>= 5 Pa	Yes	BS EN 15259	
Lowest Gas Velocity	18.8	m/s	-	-	-	
Highest Gas Velocity	20.1	m/s	-	-	-	
Ratio of Gas Velocities	1.1	: 1	< 3 : 1	Yes	BS EN 15259	
Mean Velocity	19.3	m/s	-	-	-	
Maximum angle of flow with regard to duct axis	<15	o	< 15°	Yes	BS EN 15259	
No local negative flow	Yes	-	-	Yes	BS EN 15259	

DUCT CHARACTERISTICS							
Value Units							
Shape	Circular	-					
Depth	0.60	m					
Width	-	m					
Area	0.28	m ²					
Port Depth	90	mm					

SAMPLING LINES & POINTS						
	Isokinetic	Non-Iso & Gases				
Sample port size	3.75 inch BSP	-				
Number of lines used	1	-				
Number of points / line	4	-				
Duct orientation	Vertical	-				
Filtration for TPM	In Stack	-				

SAMPLING PLATFORM					
General Platform Information					
Permanent / Temporary Platform / Ground level / Floor Level / Roof	Permanent				
Inside / Outside	Outside				

/1 Platform requirements					
Is there a sufficient working area so work can be performed in a compliant manner	Yes				
Platform has 2 levels of handrails (approximately 0.5 m & 1.0 m high)	Yes				
Platform has vertical base boards (approximately 0.25 m high)	Yes				
Platform has removable chains / self closing gates at the top of ladders	Yes				
Handrail / obstructions do not hamper insertion of sampling equipment	Yes				
Depth of Platform = >Stack depth / diameter + wall and port thickness + 1.5m	Yes				

Sampling Platform Improvement Recommendations (if applicable)

The sampling location meets all the requirements as specified in EA Guidance Note M1.



Sampling & Analytical Method Deviations

CEMEX Deviation

Due to limited production on the day of the emissions monitoring, sampling was only possible over 2 sampling periods as opposed to the 3 sampling runs the process guidance note outlines as an ideal. BS EN 13284-1 stipulates a minimum sampling duration of 30mins, in order to obtain a compliant result this minimum duration for sampling has been met, the overall effect of not obtaining a third sample (or second, change as appropriate) is seen as negligible and the result fully compliant.

Sample Points

The sampling point requirements of EN 13284-1 could not be met as one of the sample ports is siezed. As required in MID 13284-1 for such situations the number of sampling points has been doubled.

Nozzle Size

Due to the high stack velocity a nozzle less than 6mm was used.



APPENDICES

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APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

APPENDIX 3 - Measurement Uncertainty Budget Calculations



APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

MONITORING SCHEDULE								
Species	Method Standard Reference Method / Alternative Method	SOCOTEC UK Technical Procedure	UKAS Lab Number	MCERTS Accredited Method	Number of Samples			
TPM	SRM - BS EN 13284-1	AE 104	1015	Yes	2			
H_2O	SRM - BS EN 14790	AE 105	1015	Yes	1			
Velocity	SRM - BS EN ISO 16911-1	AE 154	1015	Yes	1			

Extractive Sampling



Miscellaneous

APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

CALIBRATEABLE EQUIPMENT CHECKLIST

Equipment	Equipment I.D.	Equipment	Equipment I.D.	Equipment	Equipment I.D.
Control Box DGM	LNO 13-17	Horiba PG-250 Analyser	-	Laboratory Balance	LNO 0013/0014
Box Thermocouples	LNO 03-17	FT-IR Gasmet	-	Tape Measure	LNO 18-AH
Meter In Thermocouple	LNO 03-17	FT-IR Oven Box	-	Stopwatch	LNO 17-AH
Meter Out Thermocouple	LNO 03-17	Bernath 3006 FID	-	Protractor	-
Control Box Timer	LNO 03-17	Signal 3030 FID	-	Barometer	LNO 08-AH
Oven Box	-	Servomex	-	Digital Micromanometer	-
Probe	LNO 11-08	JCT Heated Head Filter	-	Digital Temperature Meter	-
Probe Thermocouple	LNO 10-08	Thermo FID	-	Stack Thermocouple	-
Probe	-	Stackmaster	-	Mass Flow Controller	-
Probe Thermocouple	-	FTIR Heater Box for Heated Line	-	MFC Display module	-
S-Pitot	LNO 06-AH	Anemometer	-	1m Heated Line (1)	-
L-Pitot	-	Ecophysics NOx Analyser	-	1m Heated Line (2)	-
Site Balance	LNO 14-AH	Chiller (JCT/MAK 10)	-	1m Heated Line (3)	-
Last Impinger Arm	-	Heated Line Controller (1)	-	5m Heated Line (1)	-
Dioxins Cond. Thermocouple	-	Heated Line Controller (2)	-	10m Heated Line (1)	-
Callipers	LNO 31-AH	Site temperature Logger	-	10m Heated Line (2)	-
Small DGM	-		-	15m Heated Line (1)	-
Heater Controller	-		-	20m Heated Line (1)	-
Inclinometer (Swirl Device)	LNO 23-AH		-	20m Heated Line (2)	-

NOTE: If the equipment I.D is represented by a dash (-), then this piece of equipment has not been used for this test.

CALIBRATION GASES							
Gas (traceable to ISO 17025)	Cylinder I.D Number	Supplier	ppm	%	Analytical Tolerance +/- %		
-	-	-	-	-	-		

STACK EMISSIONS MONITORING TEAM

MONITORING TEAM								
Personnel	MCERTS	MCERTS		TE / H&S Qualifications and Expiry Date				
	Number	Level	Expiry	TE1	TE2	TE3	TE4	H&S
Andy Hegarty	MM 03 397	MCERTS Level 2	Jan-19	Oct-19	Dec-20	Aug-21	Dec-19	Jan-19
Lindsay Adams	MM 14 1275	MCERTS Level 2	May-21	May-20	Jul-20	Nov-20	Feb-21	Mar-19



TOTAL PARTICULATE MATTER SUMMARY							
Parameter	Sampling Times	Concentration mg/m³	Uncertainty mg/m ³	Limit mg/m³	Emission Rate g/hr		
Run 1	08:29 - 09:01 19 October 2018	29	1.2	50	447		
Run 2	09:15 - 09:47 19 October 2018	31	1.2	50	479		
Blank	-	3.7	-	-	-		

Reference conditions are 273K, 101.3kPa without correction for water vapour

Acetone Blank Value	Acceptable Value
mg/l	mg/l
2.0	10

FILTER INFORMATION

	SAMPLES							
Test	Filter & Probe Rinse Number	Filter Start Weight	Filter End Weight	Mass Gained on Filter	Probe Rinse Start Weight	Probe Rinse End Weight	Mass Gained on Probe	Combined Total Mass Gained
		g	g	g	g	g	g	g
Run 1	G8960	0.10735	0.11722	0.00987	190.84590	190.85120	0.00530	0.01517
Run 2	G8961	0.10702	0.11900	0.01198	199.98130	199.98580	0.00450	0.01648

If total mass gained is less than the LOD then the LOD is reported

BLANKS								
Test	Filter & Probe Number	Filter Start Weight	Filter End Weight	Mass Gained Filter	Probe Start Weight	Probe End Weight	Mass Gained Probe	Combined Total Mass Gained
		g	g	g	g	g	g	g
Run 1	G8991	0.10649	0.10647	-0.00002	168.35700	168.35900	0.00200	0.00198

If total mass gained is less than the LOD then the LOD is reported



APPENDIX 2 - Summaries, Calculations, Raw Data and Chart	ts
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	RUN 1			TPM
Absolute pressure of stack gas, P _s		Molecular weight of dry gas, M _d		
Barometric pressure, P _b mm Hg	769.51	CO ₂	%	0.08
Stack static pressure, P _{static} mm H ₂ C	6.12	0 ₂	%	20.90
$P_s = P_b + (P_{static})$ mm Hg	769.96	Total	%	20.98
13.6		N ₂ (100 -Total)	%	79.02
Vol. of water vapour collected, V _{wstd}		$M_d = 0.44(\%CO_2)+0.32(\%O_2)+0.28(\%N_2)$		28.85
Moisture trap weight increase,Vlc	11.0	Molecular weight of wet gas, M _s		
$V_{wstd} = (0.001246)(V_{lc})$ m ²		$M_s = M_d(1 - B_{wo}) + 18(B_{wo})$	g/gmol	28.57
Volume of gas metered dry, V _{mstd}		Actual flow of stack gas, Q _a		
Volume of gas sample through gas meter, V _m	0.534	Area of stack, A _s	m²	0.28
Gas meter correction factor, Y _d	0.981	$Q_{a} = (60)(A_{s})(V_{s})$	m³/min	331.3
Mean dry gas meter temperature, T _m	° 10.500	Total flow of stack gas, Q		
Mean pressure drop across orifice, DH mmH ₂ C	36.558	Conversion factor (K/mm.Hg)		0.3592
$V_{mstd} = (0.3592)(V_m)(P_b + (DH/13.6))(Y_d)$ m ³	0.513	$Q_{std} = (Q_a)P_s(0.3592)(1-B_{wo})$	Dry	251.9
$\frac{1}{T_m + 273}$		$(T_s) + 273$	-	
Volume of gas metered wet, V _{mstw}		$Q_{stdO2} = (Q_a)P_s(0.3592)(1-B_{wo})(O_2REF)$	@O ₂ ref	No O2 Ref
$V_{mstw} = V_{mstd} + V_{wstd}$ m ²	0.5262	(T _s) +273		
Vol. of gas metered at O ₂ Ref. Cond., V _{mstd@X%O2}		$Q_{stw} = (Q_a)P_s(0.3592)$ (T _s) +273	Wet	258.59
Is the process burning hazardous waste? (If yes, no	No	Percent isokinetic, %I		
favourable oxygen correction)	-	Nozzle diameter, D _n	mm	4.88
% oxygen measured in gas stream, act%O2	20.9	Nozzle area, A _n	mm ²	18.73
% oxygen reference condition	21	Total sampling time, g	min	32
	No O2 Ref	$%I = (4.6398E6)(T_s + 273)(V_{mstd})$	%	96.0
$\begin{array}{llllllllllllllllllllllllllllllllllll$		$\frac{(\text{Ps})(V_{s})(A_{n})(q)(1-B_{w_{0}})}{(P_{s})(V_{s})(A_{n})(q)(1-B_{w_{0}})}$	-	
$V_{mstd@X\%oxygen} = (V_{mstd}) (O_{2 Ref}) m^{2}$	No O2 Ref	Acceptable isokinetic range 95% to 115%		Yes
Moisture content, Bwo	110 02 1101	Particulate Concentration, C		100
$B_{wo} = V_{wstd}$	0.0260	Mass collected on filter, M_f	q	0.00987
$\frac{V_{\text{mstd}} + V_{\text{wstd}}}{V_{\text{mstd}} + V_{\text{wstd}}}$		Mass collected in probe, M_p	g	0.00530
Moisture by FTIR %		Total mass collected, M_n	g	0.01517
Velocity of stack gas, V _s	-	$C_{wet} = M_n$	9 mg/m³	28.827
Pitot tube velocity constant, K_p	34.97	<u></u>		201021
Velocity pressure coefficient, C_p	0.81	$C_{\text{max}} = M_{\text{max}}$	mg/m³	29.598
Mean of velocity heads, DP_{ava} mm H ₂ C		V_{mstw} $C_{dry} = \frac{M_n}{V_{mstd}}$		25.050
Mean square root of velocity heads, ÖDP	5.43	$C_{dry(0,X\%02)} = M_n$	mg/m³	No O2 Ref
Mean stack gas temperature, T_s °(V _{dry@X%02} V _{mstd@X%oxygen}		110 02 1101
$W_{s} = (K_{p})(C_{p})(\ddot{O}DP)(\ddot{O}(T_{s} + 273)) $ m/s		Particulate Emission Rates, E		
$V_s = (\frac{K_p}{(U_p)(U_p)(U_p)(U(T_s + 2T_s))})$ (11/5) (M_s)(P_s)	19.00	$E = [(C_{wet})(Q_{stw})(60)] / 1000$		447.26



APPENDIX 2 - Summaries, Calculations, Raw Data and Charts	s
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ISOKINETIC SAMPLING EQUATIONS - R	UN 2			TPM
Absolute pressure of stack gas, P _s		Molecular weight of dry gas, M_d		
Barometric pressure, P _b mm Hg	769.51	CO ₂	%	0.08
Stack static pressure, P _{static} mm H ₂ O	6.12	O ₂	%	20.90
$P_s = P_b + (P_{static})$ mm Hg	769.96	Total	%	20.98
13.6		N ₂ (100 -Total)	%	79.02
Vol. of water vapour collected, V _{wstd}		$M_d = 0.44(\%CO_2)+0.32(\%O_2)+0.28(\%N_2)$		28.85
Moisture trap weight increase,Vlc g	-	Molecular weight of wet gas, Ms		
$V_{wstd} = (0.001246)(V_{lc})$ m ³	-	$M_s = M_d(1 - B_{wo}) + 18(B_{wo})$	g/gmol	28.57
Volume of gas metered dry, V _{mstd}		Actual flow of stack gas, Q _a		
Volume of gas sample through gas meter, V_m	0.550	Area of stack, A _s	m ²	0.28
Gas meter correction factor, Y _d	0.981	$Q_a = (60)(A_s)(V_s)$	m³/min	334.1
Mean dry gas meter temperature, T _m	12.500	Total flow of stack gas, Q		
Mean pressure drop across orifice, DH mmH ₂ O	37.452	Conversion factor (K/mm.Hg)		0.3592
$V_{metd} = (0.3592)(V_m)(P_b+(DH/13.6))(Y_d)$ m ³	0.524	$Q_{std} = (Q_a)P_s(0.3592)(1-B_{wo})$	Dry	254.0
$V_{mstd} = (0.3592)(V_m)(P_b+(DH/13.6))(Y_d) \qquad m^3$ T _m + 273		$Q_{std} = \frac{(Q_a)P_s(0.3592)(1-B_{wo})}{(T_s)+273}$	-	
Volume of gas metered wet, V _{mstw}			@O ₂ ref	No O2 Ref
$V_{mstw} = V_{mstd} + V_{wstd}$ m ³	0.5383	(T _s) +273		
Vol. of gas metered at O_2 Ref. Cond., $V_{mstd@X\%02}$		$Q_{stw} = (Q_a)P_s(0.3592)$	Wet	260.82
	N -	(T _s) +273		
Is the process burning hazardous waste? (If yes, no favourable oxygen correction)	No	Percent isokinetic, %I		4.88
	20.0	Nozzle diameter, D _n	mm 2	
% oxygen measured in gas stream, act % O_2	20.9	Nozzle area, A _n	mm ²	18.73
% oxygen reference condition	21 No O2 Ref	Total sampling time, q	min %	32
$O_2 \text{ Reference} \qquad O_2 \text{ Ref} = 21.0 - \operatorname{act} \otimes O_2$ Factor $21.0 - \operatorname{ref} \otimes O_2$	NO UZ REI	%I = (4.6398E6)(T _s +273)(V _{mstd})	70	97.4
-		$(P_s)(V_s)(A_n)(q)(1-B_{wo})$		Ma a
$V_{mstd@X\%oxygen} = (V_{mstd}) (O_{2 Ref}) m^3$	No O2 Ref	Acceptable isokinetic range 95% to 115%		Yes
Moisture content, B _{wo}	0.0000	Particulate Concentration, C		0.01198
$B_{wo} = \frac{V_{wstd}}{V_{mstd} + V_{wstd}}$ %	0.0260	Mass collected on filter, M _f	g	0.00450
	2.60	Mass collected in probe, M _p	g	0.00450
	-	Total mass collected, M _n	g	
/elocity of stack gas, V _s	04.07		mg/m³	30.62
Pitot tube velocity constant, K _p	34.97	V _{mstw}		
/elocity pressure coefficient, C _p	0.81	V_{mstw} $C_{dry} = \frac{M_n}{V_{mstd}}$	mg/m³	31.44
Mean of velocity heads, DP_{avg} mm H ₂ O	30.00			
Alean square root of velocity heads, ÖDP	5.48	1	mg/m³	No O2 Ref
Mean stack gas temperature, T _s °C	81	V _{mstd@X%oxygen}		
$V_{s} = (K_{p})(C_{p})(ODP)(\sqrt{(T_{s} + 273)})$ m/s	19.69	Particulate Emission Rates, E		
$(M_s)(P_s)$		$E = [(C_{wet})(Q_{stw})(60)] / 1000$		479.13



TOTAL PARTICULATE MATTER QUALITY ASSURANCE CHECKLIST

			LEAK RATE			
	Mean Sampling	Pre-sampling	Post-sampling	Maximum	Acceptable	Leak Tests
Run	Rate	Leak Rate	Leak Rate	Vacuum	Leak Rate	Acceptable?
	litre/min	litre/min	litre/min	mm Hg	litre/min	
Run 1	16.37	0.00	0.10	-228.6	0.33	Yes
Run 2	16.86	0.10	0.00	-254	0.34	Yes

ISOKINETICITY					
Run	Isokinetic Variation %	Acceptable Isokineticity			
Run 1	96.00	Yes			
Run 2	97.36	Yes			
Acceptable isoki	netic range 95%	6 to 115%			

WEIGHING BALANCE UNCERTAINTY						
Run	Result	5% ELV	LOD < 5% ELV			
	mg/m³	mg/m³				
Run 1	0.46	2.5	Yes			
Run 2	0.45	2.5	Yes			
The above is based on both the Filter and rinse uncertainty						

Acceptable isokinetic range 95% to 115%

The above is based on both the Filter and rinse uncertainty

BLANK VALUE						
	Overall Blank	Daily Emission	Acceptable	Overall Blank		
Run	Value	Limit Value	Blank Value	Acceptable		
	mg/m ³	mg/m ³	mg/m ³	mg/m ³		
Blank 1	3.74	50	5.0	Yes		

	FILTERS						
Run	Filter Material	Filter Size	Max Filtration	Pre-use Filter Conditioning	Post-use Filter Conditioning		
			Temperature	Temperature	Temperature		
		mm	°C	°C	°C		
Run 1	Glass Fibre	47	83	180	160		
Run 2	Glass Fibre	47	83	180	160		



MOISTURE CALCULATIONS

Moisture Determination - Isokinetic								
Test Number	Sampling Time and Date	Start Weight	End Weight	Total gain	Concentration	LOD	Uncertainty	
		kg	kg	kg	%	%	%	
Run 1	08:29 - 09:01 19 October 2018	3.5460	3.5570	0.0110	2.6	0.02	3.4	

Moisture Quality Assurance							
Test Number	Sampling Duration	Total Volume Sampled	Sampling Rate	Start Leak Rate	End Leak Rate	Acceptable Leak Rate	Leak Tests Acceptable?
	mins	- I	l/min	l/min	l/min	l/min	
Run 1	32	526	16.4	0.00	0.10	0.33	Yes

PRELIMINARY STACK SURVEY

Stack Characteristics		
Stack Diameter / Depth, D	0.60	m
Stack Width, W	-	m
Stack Area, A	0.28	m ²
Average stack gas temperature	78	°C
Stack static pressure	0.06	kPa
Barometric Pressure	102.6	kPa

Component	Molar	Density	Conc	Dry Volume	Dry Conc	Conc	Wet Volume	Wet Conc
	Mass	kg/m°	Dry	Fraction	kg/m³	Wet	Fraction	kg/m³
	М	р	% Vol	r	pi	% Vol	r	pi
CO ₂	44	1.963059	0.075238	0.000752	0.001477	0.073279	0.000733	0.001439
0 ₂	32	1.427679	20.900000	0.209000	0.298385	20.355654	0.203557	0.290613
N ₂	28	1.249219	79.024762	0.790248	0.987193	76.966542	0.769665	0.961481
H ₂ O	18	0.803070	-	-	-	2.604525	0.026045	0.020916

Where: p

p = M / 22.41 pi = r x p

Calculation of Stack Gas Densities					
Determinand	Result	Units			
Dry Density (STP), P _{STD}	1.2871	kg/m ³			
Wet Density (STP), P STW	1.2744	kg/m ³			
Dry Density (Actual), P _{Actual}	1.0159	kg/m ³			
Average Wet Density (Actual), P _{ActualW}	1.006	kg/m ³			

Where:

 P_{STD} = sum of component concentrations, kg/m³ (not including water vapour) P_{STW} = (P_{STD} + p*i* of H₂O) / (1 + (p*i* of H₂O / 0.8036)) $P_{Actual} = P_{STD} x (Ts / Ps) x (Pa / Ta)$ $P_{ActualW} = P_{STW} x (Ts / Ps) x (Pa / Ta)$



PRELIMINARY STACK SURVEY

TRAVERSE 1

Date of Survey	19 October 2018
Time of Survey	08:12
Velocity Measurement Device:	S-Type Pitot

_				Sampling Line A	-			
Traverse	Distance	DP pt	DP pt	Temp	Velocity	Volumetric	0 ₂	Angle
Point	into	mmH ₂ O	Ра	°C	m/s	Flow Rate (actual)	%	of Swir
	duct (m)	(average of 3 readings)	(average of 3 readings)			M³/s	Vol	o
1	0.05	28.0	274	77	18.8	5.3	-	<15
2	0.15	32.0	314	77	20.1	5.7	-	<15
3	0.45	30.0	294	78	19.5	5.5	-	<15
4	0.55	28.0	274	78	18.8	5.3	-	<15
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
Mean	-	29.5	289	78	19.3	5.5	-	-

Sampling Line B									
Traverse	Distance	DP pt	DP pt	Temp	Velocity	Volumetric	0 ₂	Angle	
Point	into	mmH ₂ O	Ра	°C	m/s	Flow Rate (actual)	%	of Swirl	
	duct (m)	(average of 3 readings)	(average of 3 readings)			M³/s	Vol		
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
-	-	-	-	-	-	-	-	-	
Mean	-	-	-	-	-	-	-	-	

PRELIMINARY STACK SURVEY QUALITY ASSURANCE CHECKLIST

PITOT LEAK CHECK								
		Pre Traver	se Leak Rate			Post Traver	se Leak Rate	
Run	Start Value	End Value	Difference	Outcome	Start Value	End Value	Difference	Outcome
	Pa	Pa	%		Pa	Pa	%	
Run 1	96	96	0.0	Pass	102	102	0.0	Pass

To complete a compliant pitot leak check a pressure of over 80 mmH O (or 800 Pa) is applied and the pressure drop monitored over 5 mins. A drop of less than 5% must be observed.

S-Type Pitot Stagnation Check								
Run	Stagnation (Pa)	Reference (Pa)	Difference (Pa)	Outcome (Permitted +/- 10 Pa)				
Run 1	60	60	0.0	Pass				



PRELIMINARY STACK SURVEY (CONTINUED)

Sampling Plane Validation Criteria							
EA Technical Guidance Note (Monitoring) M1	Result	Units	Requirement	Compliant			
Lowest Differential Pressure	274	Pa	>= 5 Pa	Yes			
Lowest Gas Velocity	18.8	m/s	-	-			
Highest Gas Velocity	20.1	m/s	-	-			
Ratio of Gas Velocities	1.1	-	< 3 : 1	Yes			
Maximum angle of flow with regard to duct axis	<15	0	< 15°	Yes			
No local negative flow	Yes	-	-	Yes			

Calculation of Stack Gas Velocity, V
Velocity at Traverse Point, V = $K_{pt} \times (1-e) * \ddot{O}(2 * DP_{pt} / P_{ActualW})$
Where:
K _{nt} = Pitot tube calibration coefficient
F.
(1-e) = Compressibility correction factor, assumed at a constant 0.998

Average Stack Gas Velocity, Va	19.3	m/s

Calculation of Stack Gas Volumetric Flowrate, Q							
Duct gas flow conditions	Actual	Reference	Units				
Temperature	78	0	°C				
Total Pressure	102.66	101.3	kPa				
Oxygen	20.9	21	%				
Moisture	2.60	2.60	%				
Pitot tube calibration coefficient, K _{pt}	0.81						

Gas Volumetric Flowrate	Result	Units
Average Stack Gas Velocity (Va)	19.32	m/s
Stack Area (A)	0.28	m ²
Gas Volumetric Flowrate (Actual), Q _{Actual}	19667	m³/hr
Gas Volumetric Flowrate (STP, Wet), Q _{STP}	15524	m³/hr
Gas Volumetric Flowrate (STP, Dry), Q _{STP,Dry}	15120	m³/hr
Gas Volumetric Flowrate (REF), Q _{Ref}	15524	m³/hr

Where:

 $\begin{array}{l} Q_{Actual} = Va \; x \; A \; x \; 3600 \\ Q_{STP} = Q \; (Actual) \; x \; (Ts \; / \; Ta) \; x \; (Pa \; / \; Ps) \; x \; 3600 \\ Q_{STP,Dry} = Q \; (STP) \; / \; (100 \; - \; (100 \; / \; Ma)) \; x \; 3600 \\ Q_{Ref} = Q \; (STP) \; x \; ((100 \; - \; Ma) \; / \; (100 \; - \; Ms)) \; x \; ((20.9 \; - \; O_2a) \; / \; (20.9 \; - \; O_2s)) \end{array}$

Nomenclature:

Ts = Absolute Temperature, Standard Conditions, 273 K Ps = Absolute Pressure, Standard Conditions, 101.3 kPa Ta = Absolute Temperature, Actual Conditions, K Pa = Absolute Pressure, Actual Conditions, kPa Ma = Water vapour, Actual Conditions, % Vol Ms = Water vapour, Reference Conditions, % Vol O₂a = Oxygen, Actual Conditions, % Vol O₂s = Oxygen, Reference Conditions, % Vol



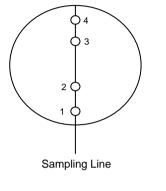
Units

-

APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

STACK DIAGRAM

	Value	Units		Non-Isokinetic/Gases San		
Stack Depth	0.60	m	Sampling	Distance	Distance int	
Stack Width	-	m	Point	(% of Depth)	Stack	
rea	0.28	m ²	-	-	-	



Isokinetic Sampling							
Sampling	Distance	Distance into	Swirl				
Point	(% of Depth)	Stack (m)	0				
1	8.3	0.05	< 15				
2	25.0	0.15	< 15				
3	75.0	0.45	< 15				
4	91.7	0.55	< 15				
-	-	-	-				
-	-	-	-				
-	-	-	-				
-	-	-	-				
-	-	-	-				
-	-	-	-				
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-	-	-	-				
-	-	-	-				
-	-	-	-				

- Ο Isokinetic sampling point
- Isokinetic sampling points not used
- igodolNon Isokinetic/Gases sampling point

SAMPLING LOCATION





4.12

%

APPENDIX 3 - Measurement Uncertainty Budget Calculations

MEASUREMENT UNCERTAINTY BUDGET - TOTAL PARTICULATE MATTER

Run	Sampled Volume	Sampled Gas Temp	Sampled Gas Pressure	Sampled Gas Humidity	Oxygen Content	Limit of Detection	Leak	Uncollected Mass
	m³	К	kPa	% by volume	% by volume	% by mass	%	mg
MU required	<u><</u> 2%	<u><</u> 2%	<u><</u> 1%	<u><</u> 1%	<u><</u> 10%	<u><</u> 5% of ELV	<u><</u> 2%	<u>< 10% of ELV</u>
Run 1	0.001	2.0	0.50	1.0	N/A	0.2400	-	-
as a %	0.20	0.56	0.49	1.0	N/A	0.91213	0.61	0.004
compliant?	Yes	Yes	Yes	Yes	N/A	Yes	Yes	Yes
Run 2	0.0011	2.0	0.50	1.0	N/A	0.240	-	-
as a %	0.20	0.70	0.49	1.0	N/A	0.892	0.00000	0.004
compliant?	Yes	Yes	Yes	Yes	N/A	Yes	Yes	Yes

Run	Volume (STP)	Mass of particulate	O ₂ Correction	Leak	Uncollected Mass	Combined uncertainty
	m³	mg	-	mg/m³	mg	
Run 1	0.40	15.1700	1.0	0.102	0.0011	-
MU as mg/m³	0.37	0.4561	-	0.102	0.0022	0.59
MU as %	1.27	1.5821	-	0.353	0.0075	-
Run 2	0.52	16.4800	1.0	0.000	0.0011	-
MU as mg/m³	0.41	0.4459	-	0.00000	0.0021	0.60
MU as %	1.3	1.4563	-	0.00000	0.0069	-
R1 - Uncertainty	expressed at a 959	% confidence le	vel (where k = 2)		1.19	mg/m³

 R2 - Uncertainty expressed at a 95% confidence level (where k = 2)
 1.21
 mg/m³
 3.95
 %

(k is a coverage factor which gives a 95% confidence in the quoted figures)

Reference - SOCOTEC UK Technical Procedure AE150 Estimation of Uncertainty of Measurement



APPENDIX 3 - Measurement Uncertainty Budget Calculations

MEASUREMENT UNCERTAINTY BUDGET - MOISTURE

Run	Sampled Volume	Sampled Gas Temp	Sampled Gas Pressure	Sampled Gas Humidity	Oxygen Content	Leak
	m³	K	kPa	% by volume	% by volume	%
MU required	<u><</u> 2%	<u><</u> 2%	<u><</u> 1%	<u><</u> 1%	<u><</u> 10%	<u><</u> 2%
Run 1	0.001	2.0	0.50	1.0	N/A	-
as a %	0.20	0.56	0.49	1.0	N/A	0.61
compliant?	Yes	Yes	Yes	Yes	N/A	Yes

Run	Volume (STP)	Mass Gained	O ₂ Correction	Leak	Uncollected Mass	Combined uncertainty
	m³	mg		mg/m³	mg	
Run 1	0.40	11000	1.0	75.69	58	-
MU as % v/v	0.03	0.02	-	0.01	0.014	0.05
MU as %	1.27	0.91	-	0.35	0.52	-

R1 - Uncertainty expressed at a 95% confidence level (where k = 2)	0.09	% v/v	3.37	%



APPENDIX 3 - Measurement Uncertainty Budget Calculations

MEASUREMENT UNCERTAINTY BUDGET - VELOCITY & VOLUMETRIC FLOW RATE

Measured Velocity at Actual Conditions	19.3	m/s
Measured Volumetric Flow rate at Actual Conditions	19667	m³/hr

Performance Characteristics & Source of Value	Units	Values	Requirement	Compliant
Uncertainty of Local Gas Velocity Determination				
Uncertainty of pitot tube coefficient	-	0.010		
Uncertainty of mean local dynamic pressures	-	0.45		
Factor loading, function of the number of measurements.	3 readings	0.591	minimum 3	Yes
Range of measurment device	ра	1000		
Resolution	ра	1.00		
Calibration uncertainty	ра	6.21	<1% of Value or 20 Pa whichever is greater	Yes
Drift	% range	0.10		
Linearity	% range	0.06	<2% of value	Yes
Uncertainty of gas density determination				
Uncertainty of molar mass determination	kg/mol	0.00003		
Uncertainty of temperature measurement	К	1.79	<1% of value	Yes
Uncertainty of absolute pressure in the duct	ра	524		
Uncertainty associated with the estimate of density	-	0.007		
Uncertainty associated with the measurement of local velocity	-	0.0002		
Uncertainty associated with the measurement of mean velocity	-	0.0002		

Measurement Uncertainty - Velocity	m/s
Combined uncertainty	0.25
Expanded uncertainty at a 95% Confidence Interval	0.49

Note - The expanded uncertainty uses a coverage factor of k = 2.

Expanded Measurement Uncertainty of Velocity at a 95% Confidence Interval	%
Expressed as a % of the Measured Velocity	1.3
Expanded uncertainty at a 95% Confidence Interval	

Measurement Uncertainty Volumetric Flow Rate	m³/hr
Combined uncertainty	520
Expanded uncertainty at a 95% Confidence Interval	1019

Note - The expanded uncertainty uses a coverage factor of k = 2.

Expanded Measurement Uncertainty of Volumetric Flow Rate at a 95% Confidence Interval	%
Expressed as a % of the Measured Volumetric Flow Rate	2.6
Expanded uncertainty at a 95% Confidence Interval	5.2

Reference - SOCOTEC UK Technical Procedure AE150 Estimation of Uncertainty of Measurement



END OF REPORT

Thank you for choosing SOCOTEC UK for your environmental monitoring needs. We hope our services have met your requirements and that you are fully satisfied with your experience of working with us, we really do value your custom and would welcome your feedback. We would appreciate it if you could take a moment to complete a short online questionnaire so that we can improve our operations and address any areas that have not met with your expectations, by clicking on the following

https://www.surveymonkey.co.uk/r/CAE_customer_feedback_weblink