STACK EMISSIONS MONITORING REPORT



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Grimsby Coated Stone
Gilbey Road
Pyewipe
Grimsby
Lincolnshire
DN31 2SJ

Permit Reference: DEFRA Process Guidance Note: PG 3/15 (12)

> Release Point: Coating Plant

Sampling Date(s): 7th November 2019

SOCOTEC Job Number:	LNO 15335
Report Date:	17th April 2019
Version:	Site
Report By:	Waheed Rasul
MCERTS Number:	MM 07 851
MCERTS Level:	MCERTS Level 2 - Team Leader
Technical Endorsements:	1, 2, 3 & 4
Report Approved By:	Mark Woodruff
MCERTS Number:	MM 03 164
Business Title:	MCERTS Level 2 - Business Manager
Technical Endorsements:	1, 2, 3 & 4
Signature:	AAL





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MONITORING OBJECTIVES

CEMEX UK Materials Limited operates a roadstone coating process at Grimsby which is subject to DEFRA Process Guidance Note PG 3/15 (12), under the Environmental Permitting Regulations 2010.

SOCOTEC LTD were commissioned by CEMEX UK Materials Limited to carry out stack emissions monitoring to determine the release of prescribed pollutants from the following Plant under normal operating conditions.

The results of these tests shall be used to demonstrate compliance with a set of emission limit values for prescribed pollutants as specified in the Plant's DEFRA Process Guidance Note, PG 3/15 (12).

Plant

Coating Plant

Operator

CEMEX UK Materials Limited Grimsby Coated Stone Gilbey Road Pyewipe Grimsby Lincolnshire DN31 2SJ

DEFRA Process Guidance Note: PG 3/15 (12)

Stack Emissions Monitoring Test House

SOCOTEC - Stockport Laboratory Unit 5 Crown Industrial Estate Kenwood Road Stockport SK5 6PH UKAS and MCERTS Accreditation Number: 1015

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E	MISSIONS SUM	MARY			
Parameter	Units	Result	Calculated Uncertainty +/-	Emission Limit Value (ELV)	MCERTS accredited result
Total Particulate Matter	mg/m³	5.4	1.70	50	1
Particulate Emission Rate	g/hr	57	17.9	-	•
Moisture	%	3.28	0.10	-	√
Stack Gas Temperature	°C	31	-	-	
Stack Gas Velocity	m/s	13.3	0.32	-	
Gas Volumetric Flow Rate (Actual)	m³/hr	13540	696	-	1
Gas Volumetric Flow Rate (STP, Wet)	m³/hr	11938	614	-	Í
Gas Volumetric Flow Rate (STP, Dry)	m³/hr	11546	594	-	
Gas Volumetric Flow Rate at Reference Conditions	m³/hr	11938	614	-	

ND = None Detected,

Results at or below the limit of detection are highlighted by bold italic text.

The above volumetric flow rate is calculated using data from the preliminary survey. Mass emissions for non isokinetic tests are calculated using these values. For all isokinetic testing the mass emission is calculated using test specific flow data and not the above values.

Reference conditions are 273K, 101.3kPa without correction for water vapour



MONITORING TIMES						
Parameter	Sampling Date(s)	Sampling Times	Sampling Duration			
Total Particulate Matter Run 1	07 November 2019	07:58 - 08:30	32 minutes			
Total Particulate Matter Run 2	07 November 2019	08:55 - 09:27	32 minutes			
Preliminary Stack Traverse	07 November 2019	07:20	-			



PROCESS DETAILS

Parameter	Process Details
Description of process	Roadstone Coating
Continuous or batch	Continuous
Product Details	20mm
Part of batch to be monitored (if applicable)	When mixing
Normal load, throughput or continuous rating	26 t/hr
Fuel used during monitoring	Kerosene
Abatement	Bag Filter
Plume Appearance	Slight Plume Visible



Monitoring Methods

The selection of standard reference / alternative methods employed by SOCOTEC is determined, wherever possible by the hierarchy of method selection outlined in Environmental Protection Agency Technical Guidance Note (Monitoring) AG2.

		MON	TORING METH	ODS			
Species	Method Standard Reference Method / Alternative Method	SOCOTEC Technical Procedure	UKAS Lab Number	MCERTS Accredited Method	Limit of Detection (LOD)	Calculated MU +/- % Result	Calculated MU +/- % ELV
Total Particulate Matter	SRM - EN 13284-1	AE 104	1015	Yes	0.35 mg/m³	31.4%	1.5%
Moisture	SRM - BS EN 14790	AE 063	1015	Yes	0.02%	3.11%	N/A - No ELV
Velocity	SRM - EN ISO 16911-1	AE 154	1015	Yes	5 Pa	2.4%	N/A - No ELV
Volumetric Flow Rate	SRM - EN ISO 16911-1	AE 154	1015	Yes	-	5.1%	N/A - No ELV



Analytical Methods

The following tables list the analytical methods employed together with the custody details. Unless otherwise stated the samples are archived at the analysis lab location.

SAMPLING METHODS WITH SUBSEQUENT ANALYSIS							
Species	Analytical Technique	Analytical Procedure	UKAS Lab Number	UKAS Accredited Lab Analysis	Analysis Lab	Analysis Report number	Archive Period
Total Particulate Matter	Gravimetric	AE 106	1015	Yes	SOCOTEC (Stockport)	N/A	8 Weeks

ON-SITE TESTING							
Species	Analytical Technique	Analytical Procedure	UKAS Lab Number	MCERTS Accredited Analysis	Laboratory	Data Archive Location	Archive Period
Moisture	Gravimetric	AE 105	1015	Yes	SOCOTEC (Stockport)	-	-



SAM	IPLING LOCAT	ION			
Sampling Plane Validation Criteria	Value	Units	Requirement	Compliant	Method
Lowest Differential Pressure	138	Pa	>= 5 Pa	Yes	EN 15259
Lowest Gas Velocity	13.2	m/s	-	-	-
Highest Gas Velocity	13.4	m/s	-	-	-
Ratio of Gas Velocities	1.0	: 1	< 3 : 1	Yes	EN 15259
Mean Velocity	13.3	m/s	-	-	-
Maximum angle of flow with regard to duct axis	<15	o	< 15°	Yes	EN 15259
No local negative flow	Yes	-	-	Yes	EN 15259

DUCT CHARACTERISTICS					
	Value	Units			
Shape	Circular	-			
Depth	0.60	m			
Width	-	m			
Area	0.28	m ²			
Port Depth	90	mm			

SAMPLING LINES & POINTS					
	Isokinetic	Non-Iso & Gases			
Sample port size	3.75 inch port	-			
Number of lines used	1	-			
Number of points / line	4	-			
Duct orientation	Vertical	-			
Filtration for TPM	In Stack	-			

SAMPLING PLATFORM		
General Platform Information		
Permanent / Temporary Platform / Ground level / Floor Level / Roof	Permanent	
Inside / Outside	Outside	

AG1 Platform requirements	
Is there a sufficient working area so work can be performed in a compliant manner	Yes
Platform has 2 levels of handrails (approximately 0.5 m & 1.0 m high)	Yes
Platform has vertical base boards (approximately 0.25 m high)	Yes
Platform has removable chains / self closing gates at the top of ladders	Yes
Handrail / obstructions do not hamper insertion of sampling equipment	Yes
Depth of Platform = >Stack depth / diameter + wall and port thickness + 1.5m	Yes

Sampling Platform Improvement Recommendations (if applicable)

The sampling location meets all the requirements as specified in EA Guidance Note M1.



Sampling & Analytical Method Deviations

Sample Runs

Due to limited production on the day of the emissions monitoring, sampling was only possible over 2 sampling periods as opposed to the 3 sampling runs the process guidance note outlines as an ideal. BS EN 13284-1 stipulates a minimum sampling duration of 30mins, in order to obtain a compliant result this minimum duration for sampling has been met, the overall effect of not obtaining a third sample (or second, change as appropriate) is seen as negligible and the result fully compliant.","Due to limited production on the day of the emissions monitoring

Sample Points

The sampling point requirements of EN 13284-1 could not be met as one of the sample ports is siezed. As required in MID 13284-1 for such situations the number of sampling points has been doubled.



APPENDICES

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APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

MONITORING SCHEDULE									
Species	Method Standard Reference Method / Alternative Method	SOCOTEC Technical Procedure	UKAS Lab Number	MCERTS Accredited Method	Number of Samples				
Total Particulate Matter	SRM - EN 13284-1	AE 104	1015	Yes	2				
Moisture	SRM - BS EN 14790	AE 063	1015	Yes	1				
Velocity	SRM - EN ISO 16911-1	AE 154	1015	Yes	1				

Extractive Sampling



Miscellaneous

APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

CALIBRATEABLE EQUIPMENT CHECKLIST

		motumental Palaryo				
Equipment	Equipment I.D.	Equipment	Equipment I.D.	Equipment	Equipment I.D.	
Control Box DGM	LNO 13-23	Horiba PG-250 Analyser	-	Laboratory Balance	LNO 0013/0014	
Box Thermocouples	LNO 03-23	FT-IR Gasmet	-	Tape Measure	LNO 18-WR	
Meter In Thermocouple	LNO 03-23	FT-IR Oven Box	-	Stopwatch	LNO 17-WR	
Meter Out Thermocouple	LNO 03-23	Bernath 3006 FID	-	Protractor	-	
Control Box Timer	LNO 17-23	Signal 3030 FID	-	Barometer	LNO 08-WR	
Oven Box	-	Servomex	-	Digital Micromanometer	-	
Probe	LNO 11-05	JCT Heated Head Filter	-	Digital Temperature Meter	-	
Probe Thermocouple	LNO 10-05	Thermo FID	-	Stack Thermocouple	-	
Probe	-	Stackmaster	-	Mass Flow Controller	-	
Probe Thermocouple	-	FTIR Heater Box for Heated Line	-	MFC Display module	-	
S-Pitot	LNO 06-JO	Anemometer	-	1m Heated Line (1)	-	
L-Pitot	-	Ecophysics NOx Analyser	-	1m Heated Line (2)	-	
Site Balance	LNO 14-JO	Chiller (JCT/MAK 10)	-	1m Heated Line (3)	-	
Last Impinger Arm	-	Heated Line Controller (1)	-	5m Heated Line (1)	-	
Dioxins Cond. Thermocouple	-	Heated Line Controller (2)	-	10m Heated Line (1)	-	
Callipers	LNO JO	Site temperature Logger	-	10m Heated Line (2)	-	
Small DGM	-		-	15m Heated Line (1)	-	
Heater Controller	-		-	20m Heated Line (1)	-	
Inclinometer (Swirl Device)	LNO 23-JO		-	20m Heated Line (2)	-	

NOTE: If the equipment I.D is represented by a dash (-), then this piece of equipment has not been used for this test.

CALIBRATION / CHECK GASES									
Gas (traceable to ISO 17025) Cylinder I.D Number		Supplier	ppm	%	Analytical Tolerance +/- %				
-	-	-	-	-	-				

STACK EMISSIONS MONITORING TEAM

MONITORING TEAM										
Personnel	MCERTS	MC	ERTS	TE / H&S Qualifications and Expiry Date						
Personner	Number	Level	Expiry	TE1	TE2	TE3	TE4	H&S		
Waheed Rasul	MM 07 851	MCERTS Level 2	Mar-20	Dec-23	Jun-20	Dec-20	Mar-20	Mar-22		
Pete Watson	MM 08 953	MCERTS Level 1	Jun-21	-	-	-	-	Jun-21		



TOTAL PARTICULATE MATTER SUMMARY									
Parameter	Sampling Times	Concentration mg/m³	Uncertainty mg/m³	ELV mg/m³	Emission Rate g/hr				
Run 1	07:58 - 08:30 07 November 2019	1.3	0.71	50	14				
Run 2	08:55 - 09:27 07 November 2019	9.5	0.77	50	100				
Blank	-	0.35	-	-	-				

Reference conditions are 273K, 101.3kPa without correction for water vapour

Acetone Blank Value	Acceptable Value
mg/l	mg/l
2.0	10

FILTER INFORMATION

SAMPLES											
Test	Filter & Probe Rinse Number	Filter Start Weight	Filter End Weight	Mass Gained on Filter	Probe Rinse Start Weight	Probe Rinse End Weight	Mass Gained on Probe	Combined Total Mass Gained			
		g	g	g	g	g	g	g			
Run 1	G9839	0.11079	0.11126	0.00047	202.95780	202.95810	0.00030	0.00077			
Run 2	G9840	0.10716	0.10737	0.00021	208.09020	208.09550	0.00530	0.00551			

If total mass gained is less than the LOD then the LOD is reported

BLANKS											
Test	Filter & Probe Number	Filter Start Weight	Filter End Weight	Mass Gained Filter	Probe Start Weight	Probe End Weight	Mass Gained Probe	Combined Total Mass Gained			
		g	g	g	g	g	g	g			
Run 1	G9737	0.10751	0.10742	-0.00009	182.94170	182.93900	-0.00270	0.00021			

If total mass gained is less than the LOD then the LOD is reported



ISOKINETIC SAMPLING EQUATION	ONS - R	UN 1			TPM
Absolute pressure of stack gas, P _s			Molecular weight of dry gas, M _d		
Barometric pressure, P _b	Кра	99.3	CO ₂	%	0.08
Stack static pressure, P _{static}	pa	150	02	%	20.90
$P_s = P_b + P_{static}$	Кра	99.5	Total	%	20.98
· s · D · static			N ₂ (100 -Total)	%	79.02
Vol. of water vapour collected, V _{wstd}			$M_d = 0.44(\%CO_2)+0.32(\%O_2)+0.28(\%N_2)$		28.85
Moisture trap weight increase, Vic	g	15.7	Molecular weight of wet gas, Me		20.00
V _{wstd} = (0.001246)(V _{lc})	m ³	0.0195622	$M_s = M_d(1 - B_{wo}) + 18(B_{wo})$	g/gmol	28.49
Volume of gas metered dry, V _{mstd}		0.0190022	Actual flow of stack gas, Q _a	g, ginor	20.15
Volume of gas sample through gas meter, V_m		0.626	Area of stack, A _s	m ²	0.28
Gas meter correction factor, Y_d		0.990	$Q_a = (60)(A_s)(V_s)$	m³/min	218.7
Mean dry gas meter temperature, T_m		289	Total flow of stack gas, Q	111 / 11111	210.7
Mean pressure drop across orifice, DH	mmH₂0	37.097	Conversion factor (K/mm.Hg)		0.3592
• • •	m^3	0.577	·	Dru	175.4
$V_{mstd} = (0.3592)(V_m)(P_b+(DH/13.6))(Y_d)$	m	0.577	$Q_{std} = \frac{(Q_a)P_s(0.3592)(1-B_{wo})}{(T_s)}$	Dry	175.4
Volume of gas metered wet, V _{mstw}			(3/	⊚0 rof	No 02 Pof
-	m ³	0 5062	$Q_{std02} = (Q_a)P_s(0.3592)(1-B_{wo})(O_2REF)$	@O ₂ ref	No O2 Ref
$V_{mstw} = V_{mstd} + V_{wstd}$	m	0.5962	(T_s)	Wet	101 40
Vol. of gas metered at O ₂ Ref. Cond., V _{mstd}	@X%02		$Q_{stw} = (Q_a)P_s(0.3592)$	Wet	181.40
		N.	(T _s)		
Is the process burning hazardous waste? (If yes, r	10	No	Percent isokinetic, %I		5.00
favourable oxygen correction)			Nozzle diameter, D _n	mm	5.88
% oxygen measured in gas stream, act%O	2	20.9	Nozzle area, A _n	mm ²	27.19
% oxygen reference condition		21	Total sampling time, q	min	32
O_2 Reference O_2 Ref = 21.0 - act% O_2		No O2 Ref	$%I = (4.6398E6)(T_s)(V_{mstd})$	%	106.8
Factor 21.0 - ref%O ₂			$(P_s)(V_s)(A_n)(q)(1-B_{wo})$		
V _{mstd@X%oxygen} = (V _{mstd}) (O _{2 Ref})	m³	No O2 Ref	Acceptable isokinetic range 95% to 118	5%	Yes
Moisture content, B _{wo}			Particulate Concentration, C		
$B_{wo} = \frac{V_{wstd}}{V_{mstd} + V_{wstd}}$		0.0328	Mass collected on filter, M _f	g	0.00047
V _{mstd} + V _{wstd}	%	3.28	Mass collected in probe, M _p	g	0.00030
Moisture by FTIR	%	-	Total mass collected, M _n	g	0.00077
Velocity of stack gas, V _s	Т		C _{wet} = M _n	mg/m³	1.292
Velocity pressure coefficient, C _p		0.84			
Mean of velocity heads, DP _{avg}	Pa	124.22	$C_{dry} = M_n$	mg/m³	1.335
Mean stack gas temperature, T _s	к	323	$\frac{V_{mstw}}{C_{dry} = \frac{M_n}{V_{mstd}}}$		
Gas density _(wet, ambient) , p			C _{dry@X%02} = M _n	mg/m³	No O2 Ref
p=(Ms*Ps)/(8.314*Ts)	kg/m ³	1.055	V _{mstd@X%oxygen}	-	
Stack Velocity, Vs $\Delta DPavg$	-		Particulate Emission Rates, E		
Stack Velocity, Vs $V_s = Cp \sqrt{\frac{\Delta DPavg}{p}}$	m/s	12.89	$E = [(C_{wet})(Q_{stw})(60)] / 1000$		14.06



APPENDIX 2 - Summaries, Calculations, Raw Data and Charts	s
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ISOKINETIC SAMPLING EQUAT	IONS - R	UN 2			TPI
Absolute pressure of stack gas, P _s			Molecular weight of dry gas, M _d		
Barometric pressure, P _b	Кра	99.3	CO ₂	%	0.08
Stack static pressure, P _{static}	ра	150	02	%	20.90
$P_s = P_b + P_{static}$	Кра	99.5	Total	%	20.98
	-		N ₂ (100 -Total)	%	79.02
/ol. of water vapour collected, V _{wstd}			$M_d = 0.44(\%CO_2)+0.32(\%O_2)+0.28(\%N_2)$		28.85
Moisture trap weight increase,VIc	g	-	Molecular weight of wet gas, Ms		
V _{wstd} = (0.001246)(V _{lc})	m ³	-	$M_s = M_d(1 - B_{wo}) + 18(B_{wo})$	g/gmol	28.49
/olume of gas metered dry, V _{mstd}			Actual flow of stack gas, Q _a	5 5	
/olume of gas sample through gas meter, V_m		0.614	Area of stack, A _s	m ²	0.28
Gas meter correction factor, Y _d		0.990	$Q_{a} = (60)(A_{s})(V_{s})$	m³/min	219.4
Mean dry gas meter temperature, T _m		291	Total flow of stack gas, Q		
Mean pressure drop across orifice, DH	mmH ₂ 0	33.137	Conversion factor (K/mm.Hg)		0.3592
$V_{mstd} = (0.3592)(V_m)(P_b+(DH/13.6))(Y_d)$	m ³	0.560	$Q_{std} = (Q_a)P_s(0.3592)(1-B_{wo})$	Dry	169.2
T _m			$(T_{\rm s})$	-	
/olume of gas metered wet, V _{mstw}			$Q_{stdO2} = (Q_a)P_s(0.3592)(1-B_{wo})(O_2REF)$	@O ₂ ref	No O2 Ref
$V_{\rm mstw} = V_{\rm mstd} + V_{\rm wstd}$	m ³	0.5787	(T _s)	0.2	
			$Q_{stw} = (Q_a)P_s(0.3592)$	Wet	174.93
Vol. of gas metered at O_2 Ref. Cond., V_m	std@X%O2		(T _s)		
s the process burning hazardous waste? (If ye	s, no	No	Percent isokinetic, %I		
avourable oxygen correction)			Nozzle diameter, D _n	mm	5.88
% oxygen measured in gas stream, act%	02	20.9	Nozzle area, A _n	mm ²	27.19
% oxygen reference condition		21	Total sampling time, q	min	32
$D_2 \text{ Reference} \qquad O_2 \text{ Ref = } 21.0 - \text{act%C}$ Factor $21.0 - \text{ref\%O}_2$	2	No O2 Ref	$%I = (4.6398E6)(T_s)(V_{mstd})$	%	107.5
Factor 21.0 - ref%O ₂			$(P_{s})(V_{s})(A_{n})(q)(1-B_{wo})$		
V _{mstd@X%oxygen} = (V _{mstd}) (O _{2 Ref})	m ³	No O2 Ref	Acceptable isokinetic range 95% to 11	5%	Yes
Moisture content, B _{wo}			Particulate Concentration, C		
B _{wo} = V _{wstd}		0.0328	Mass collected on filter, M _f	g	0.00021
$B_{wo} = \underbrace{V_{wstd}}_{V_{mstd}} + V_{wstd}$	%	3.28	Mass collected in probe, M _p	g	0.00530
Moisture by FTIR	%	-	Total mass collected, M _n	g	0.00551
Velocity of stack gas, V _s			C = M.	mg/m³	9.521
Velocity pressure coefficient, C _p		0.84	$C_{wet} = M_n / V_{mstw}$	-	
Mean of velocity heads, DP _{avg}	Pa	120.17	C _{dry} = M _n	mg/m³	9.844
Mean stack gas temperature, T _s	к	336	$C_{dry} = \frac{M_n}{V_{mstw}}$ $C_{dry} = \frac{M_n}{V_{mstd}}$	-	
Gas density _(wet. ambient) , p			$C_{dry@X\%O2} = M_n$	mg/m³	No O2 Ref
p=(Ms*Ps)/(8.314*Ts)	kg/m ³	1.014	V _{mstd@X%oxygen}	.	
		-	Particulate Emission Rates, E		
Stack Velocity, Vs $V_s = Cp \left \frac{\Delta DPavg}{p} \right $	m/s	12.93	$E = [(C_{wet})(Q_{stw})(60)] / 1000$		99.93



TOTAL PARTICULATE MATTER QUALITY ASSURANCE CHECKLIST

			LEAK RATE			
Run	Mean Sampling Rate	Pre-sampling Leak Rate	Post-sampling Leak Rate	Maximum Vacuum	Acceptable Leak Rate	Leak Tests Acceptable?
	litre/min	litre/min	litre/min	mm Hg	litre/min	
Run 1	19.36	0.15	-	-381	0.39	Yes
Run 2	18.99	0.15	-	3.81	0.38	Yes

In BS EN 13284-1:2017 a post sampling leak check is not require.

ISOKINETICITY							
Run	Isokinetic Variation %	Acceptable Isokineticity					
Run 1	106.81	Yes					
Run 2	107.52	Yes					
Acceptable isok	inetic range 95%	6 to 115%					

	WEIGHING BALANCE UNCERTAINTY								
Result	5% ELV	LOD < 5% ELV							
mg/m³	mg/m³								
0.35	2.5	Yes							
0.36	2.5	Yes							
	mg/m ³ 0.35 0.36	mg/m ³ mg/m ³ 0.35 2.5							

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The above is based on both the Filter and rinse uncertainty

BLANK VALUE							
	Overall Blank	Daily Emission	Acceptable	Overall Blank			
Run	Value	Limit Value	Blank Value	Acceptable			
	mg/m ³	mg/m ³	mg/m ³	mg/m ³			
Blank 1	0.35	50	5.0	Yes			

	FILTERS								
Run	Filter Material	Filter Size	Max Filtration	Pre-use Filter Conditioning	Post-use Filter Conditioning				
			Temperature	Temperature	Temperature				
		mm	°C	°C	°C				
Run 1	Glass Fibre	47	53	180	160				
Run 2	Glass Fibre	47	63	180	160				



MOISTURE CALCULATIONS

Moisture Determination - Isokinetic										
Test Number	Sampling Time and Date	Start Weight	End Weight	Total gain	Concentration	LOD	Uncertainty			
		kg	kg	kg	%	%	%			
Run 1	07:58 - 08:30 07 November 2019	3.5231	3.5388	0.0157	3.3	0.02	3.1			

Moisture Quality Assurance								
Test Number	Sampling Duration	Total Volume Sampled	Sampling Rate	Start Leak Rate	End Leak Rate	Acceptable Leak Rate	Leak Tests Acceptable?	
	mins	1	l/min	l/min	l/min	l/min		
Run 1	32	596	19.4	0.15	-	0.39	Yes	

PRELIMINARY STACK SURVEY

Stack Characteristics					
Stack Diameter / Depth, D	0.60	m			
Stack Width, W	-	m			
Stack Area, A	0.28	m ²			
Average stack gas temperature	31	°C			
Stack static pressure	0.15	kPa			
Barometric Pressure	99.3	kPa			

tack Gas Comp	osition & Mole	cular Weights						
Component	Molar	Density	Conc	Dry Volume	Dry Conc	Conc	Wet Volume	Wet Conc
	Mass	kg/m³	Dry	Fraction	kg/m³	Wet	Fraction	kg/m³
	М	р	% Vol	r	pi	% Vol	r	pi
CO ₂	44	1.963059	0.075238	0.000752	0.001477	0.072769	0.000728	0.001429
02	32	1.427679	20.900000	0.209000	0.298385	20.214191	0.202142	0.288594
N ₂	28	1.249219	79.024762	0.790248	0.987193	76.431658	0.764317	0.954799
H ₂ O	18	0.803070	-	-	-	3.281382	0.032814	0.026352

Where:

p = M / 22.41 pi = r x p

Calculation of Stack Gas Densities						
Determinand	Result	Units				
Dry Density (STP), P _{STD}	1.2871	kg/m ³				
Wet Density (STP), P _{STW}	1.2712	kg/m ³				
Dry Density (Actual), P _{Actual}	1.1347	kg/m ³				
Average Wet Density (Actual), P _{ActualW}	1.121	kg/m ³				

Where:

 P_{STD} = sum of component concentrations, kg/m³ (not including water vapour) P_{STW} = (P_{STD} + p*i* of H₂O) / (1 + (p*i* of H₂O / 0.8036)) $P_{Actual} = P_{STD} x (Ts / Ps) x (Pa / Ta)$ $P_{ActualW} = P_{STW} x (Ts / Ps) x (Pa / Ta)$



PRELIMINARY STACK SURVEY

TRAVERSE 1

Date of Survey	07 November 2019
Time of Survey	07:20
Velocity Measurement Device:	S-Type Pitot

Traverse	Distance	DP pt	DP pt	Temp	Velocity	Volumetric	0 ₂	Angle
Point	into	Pa	mmH₂0	°C	m/s	Flow Rate (actual)	%	of Swirl
	duct (m)	(average of 3 readings)	(average of 3 readings)			m³/s	Vol	o
1	0.05	138.5	14.1	31	13.2	3.7	-	<15
2	0.15	140.5	14.3	31	13.3	3.8	-	<15
3	0.45	141.1	14.4	31	13.3	3.8	-	<15
4	0.55	142.1	14.5	31	13.4	3.8	-	<15
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
Mean	-	140.5	14.3	31	13.3	3.8	-	-

				Sampling Line B				
Traverse	Distance	DP pt	DP pt	Temp	Velocity	Volumetric	0 ₂	Angle
Point	into	Pa	mmH ₂ O	°C	m/s	Flow Rate (actual)	%	of Swirl
	duct (m)	(average of 3 readings)	(average of 3 readings)			m³/s	Vol	o
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
-	-	-	-	-	-	-	-	-
Mean	-	-	-	-	-	-	-	-

PRELIMINARY STACK SURVEY QUALITY ASSURANCE CHECKLIST

	PITOT LEAK CHECK									
	Pre Traverse Leak Rate				Post Traverse Leak Rate					
Run	Start Value	End Value	Difference	Outcome	Start Value	End Value	Difference	Outcome		
	mmH2O	mmH2O	%		mmH2O	mmH2O	%			
Run 1	140	138	1.4	Pass	165	161	2.4	Pass		

To complete a compliant pitot leak check a pressure of over 80 mmH₂O (or 800 Pa) is applied and the pressure drop monitored over 5 mins. A drop of less than 5% must be observed.

	S-Type Pitot Stagnation Check								
Rui		Stagnation (Pa)	Reference (Pa)	Difference (Pa)	Outcome (Permitted +/- 10 Pa)				
Run	1	150	150	0.0	Pass				



PRELIMINARY STACK SURVEY (CONTINUED)

Sampling Plane Validation Criteria								
EA Technical Guidance Note (Monitoring) M1	Result	Units	Requirement	Compliant				
Lowest Differential Pressure	139	Pa	>= 5 Pa	Yes				
Lowest Gas Velocity	13.2	m/s	-	-				
Highest Gas Velocity	13.4	m/s	-	-				
Ratio of Gas Velocities	1.0	-	< 3 : 1	Yes				
Maximum angle of flow with regard to duct axis	<15	0	< 15°	Yes				
No local negative flow	Yes	-	-	Yes				

Calculation of Stack Gas	Velocity, V	
Velocity at Traverse Point, V = $K_{pt} \times (1-e) \times O(2 \times DF)$	P _{pt} / P _{ActualW})	
Where:		
K_{pt} = Pitot tube calibration coefficient		
(1-e) = Compressibility correction factor, assumed	at a constant 0.99	98
Average Stack Gas Velocity, Va	13.3	m

Calculation of Stack Gas Volumetric Flowrate, Q							
Duct gas flow conditions	Actual	Reference	Units				
Temperature	31	0	°C				
Total Pressure	99.45	101.3	kPa				
Oxygen	20.9	21	%				
Moisture	3.28	3.28	%				
Pitot tube calibration coefficient, K_{pt}	0.84						

Gas Volumetric Flowrate	Result	Units
Average Stack Gas Velocity (Va)	13.30	m/s
Stack Area (A)	0.28	m²
Gas Volumetric Flowrate (Actual), Q _{Actual}	13540	m³/hr
Gas Volumetric Flowrate (STP, Wet), Q _{STP}	11938	m³/hr
Gas Volumetric Flowrate (STP, Dry), Q _{STP,Dry}	11546	m³/hr
Gas Volumetric Flowrate (REF), Q _{Ref}	11938	m³/hr

Where:

 $\begin{array}{l} Q_{Actual} = Va \; x \; A \; x \; 3600 \\ Q_{STP} = Q \; (Actual) \; x \; (Ts \; / \; Ta) \; x \; (Pa \; / \; Ps) \; x \; 3600 \\ Q_{STP,Dry} = Q \; (S1P) \; / \; (100 \; - \; (100 \; / \; Ma)) \; x \; 3600 \\ Q_{Ref} = Q \; (STP) \; x \; ((100 \; - \; Ma) \; / \; (100 \; - \; Ms)) \; x \; ((21 \; - \; O_2a) \; / \; (21 \; - \; O_2s)) \end{array}$

Nomenclature:

Ts = Absolute Temperature, Standard Conditions, 273 K Ps = Absolute Pressure, Standard Conditions, 101.3 kPa Ta = Absolute Temperature, Actual Conditions, K Pa = Absolute Pressure, Actual Conditions, kPa Ma = Water vapour, Actual Conditions, % Vol Ms = Water vapour, Reference Conditions, % Vol O₂a = Oxygen, Actual Conditions, % Vol O₂s = Oxygen, Reference Conditions, % Vol



STACK DIAGRAM

	Value	Value Units Non-Isokinetic/Gases				
Stack Depth	0.60	m				
Stack Width	-	m				
Area	0.28	m ²				

	Isokinetic Sampling									
Sampling	Distance	Distance into	Swirl							
Point	(% of Depth)	Stack (m)	ο							
1	8.3	0.05	< 15							
2	25.0	0.15	< 15							
3	75.0	0.45	< 15							
4	91.7	0.55	< 15							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
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-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							
-	-	-	-							

O Isokinetic sampling point

- Isokinetic sampling points not used
- Non Isokinetic/Gases sampling point

SAMPLING LOCATION



APPENDIX 3 - Measurement Uncertainty Budget Calculations

MEASUREMENT UNCERTAINTY BUDGET - TOTAL PARTICULATE MATTER

Run	Sampled Volume	Sampled Gas Temp	Sampled Gas Pressure	Sampled Gas Humidity	Oxygen Content	Limit of Detection	Leak	Uncollected Mass
	m³	К	kPa	% by volume	% by volume	% by mass	%	mg
MU required	<u><</u> 2%	<u><</u> 2%	<u><</u> 1%	<u><</u> 1%	<u><</u> 10%	<u><</u> 5% of ELV	<u><</u> 2%	< 10% of ELV
Run 1	0.001	2.0	0.50	1.0	N/A	0.2100	-	-
as a %	0.17	0.62	0.50	1.0	N/A	0.70451	0.77	0.000
compliant?	Yes	Yes	Yes	Yes	N/A	Yes	Yes	Yes
Run 2	0.001157469	2.0	0.50	1.0	N/A	0.210	-	-
as a %	0.20	0.69	0.50	1.0	N/A	0.726	0.79	0.000
compliant?	Yes	Yes	Yes	Yes	N/A	Yes	Yes	Yes

Run	Volume (STP)	Mass of particulate	O ₂ Correction	Leak	Uncollected Mass	Combined uncertainty
	m³	mg	-	mg/m³	mg	
Run 1	0.48	0.7700	1.0	0.006	0.0001	-
MU as mg/m°	0.02	0.3523	-	0.006	0.0002	0.35
MU as %	1.30	27.2727	-	0.447	0.0157	-
Run 2	0.53	5.5100	1.0	0.043	0.0001	-
MU as mg/m³	0.13	0.3629	-	0.043	0.0002	0.39
MU as %	1.3	3.8113	-	0.456	0.0022	-

R1 - Uncertainty expressed at a 95% confidence level (where k = 2)	0.71	mg/m³	54.61	% Result	1.41	% ELV
R2 - Uncertainty expressed at a 95% confidence level (where k = 2)	0.77	mg/m³	8.13	% Result	1.55	% ELV

(k is a coverage factor which gives a 95% confidence in the quoted figures)

Reference - SOCOTEC Technical Procedure AE150 Estimation of Uncertainty of Measurement



APPENDIX 3 - Measurement Uncertainty Budget Calculations

MEASUREMENT UNCERTAINTY BUDGET - MOISTURE

Run	Sampled Volume	Sampled Gas Temp	Sampled Gas Pressure	Sampled Gas Humidity	Oxygen Content	Leak
	m³	К	kPa	% by volume	% by volume	%
MU required	<u><</u> 2%	<u><</u> 2%	<u><</u> 1%	<u><</u> 1%	<u><</u> 10%	<u><</u> 2%
Run 1	0.001	2.0	0.50	1.0	N/A	-
as a %	0.17	0.62	0.50	1.0	N/A	0.77
compliant?	Yes	Yes	Yes	Yes	N/A	Yes

Run	Volume (STP)	Mass Gained	O ₂ Correction	Leak	Uncollected Mass	Combined uncertainty
	m³	mg	-	mg/m³	mg	
Run 1	0.48	15700	1.0	121.80	58	-
MU as % v/v	0.04	0.02	-	0.02	0.013	0.05
MU as %	1.30	0.64	-	0.45	0.37	-

R1 - Uncertainty expressed at a 95% confidence level (where k = 2)	0.11	% v/v	3.11	%
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APPENDIX 3 - Measurement Uncertainty Budget Calculations

MEASUREMENT UNCERTAINTY BUDGET - VELOCITY & VOLUMETRIC FLOW RATE

Measured Velocity at Actual Conditions	13.3	m/s
Measured Volumetric Flow rate at Actual Conditions	13540	m³/hr

Performance Characteristics & Source of Value	Units	Values	Requirement	Compliant
Uncertainty of Local Gas Velocity Determination				
Uncertainty of pitot tube coefficient	-	0.010		
Uncertainty of mean local dynamic pressures	-	1.18		
Factor loading, function of the number of measurements.	3 readings	0.591	minimum 3	Yes
Range of measurment device	ра	1000		
Resolution	ра	1.00		
Calibration uncertainty	ра	22.21	<1% of Value or 20 Pa whichever is greater	Yes
Drift	% range	0.10		
Linearity	% range	0.06	<2% of value	Yes
Uncertainty of gas density determination				
Uncertainty of molar mass determination	kg/mol	0.00003		
Uncertainty of temperature measurement	К	1.55	<1% of value	Yes
Uncertainty of absolute pressure in the duct	ра	507		
Uncertainty associated with the estimate of density	-	0.007		
Uncertainty associated with the measurement of local velocity	-	0.0001		
Uncertainty associated with the measurement of mean velocity	-	0.0002		

Measurement Uncertainty - Velocity	m/s
Combined uncertainty	0.17
Expanded uncertainty at a 95% Confidence Interval	0.32

Note - The expanded uncertainty uses a coverage factor of k = 2.

Expanded Measurement Uncertainty of Velocity at a 95% Confidence Interval	%
Expressed as a % of the Measured Velocity	1.2
Expanded uncertainty at a 95% Confidence Interval	2.4
Massurement Incortainty Volumetric Flow Pate	

Measurement Oncertainty volumetric Flow Rate	m³/hr
Combined uncertainty	355
Expanded uncertainty at a 95% Confidence Interval	
	-

Note - The expanded uncertainty uses a coverage factor of k = 2.

Expanded Measurement Uncertainty of Volumetric Flow Rate at a 95% Confidence Interval	%
Expressed as a % of the Measured Volumetric Flow Rate	2.6
Expanded uncertainty at a 95% Confidence Interval	5.1

Reference - SOCOTEC Technical Procedure AE150 Estimation of Uncertainty of Measurement



END OF REPORT

Thank you for choosing SOCOTEC for your environmental monitoring needs. We hope our services have met your requirements and that you are fully satisfied with your experience of working with us, we really do value your custom and would welcome your feedback. We would appreciate it if you could take a moment to complete a short online questionnaire so that we can improve our operations and address any areas that have not met with your expectations, by clicking on the following

https://www.surveymonkey.co.uk/r/CAE_customer_feedback_weblink